IN THE CLAIMS:

Amend Claims 91, 97, 98, 100-107, 109 and 110 as follow:

Claims 1-90. Canceled

91. (Currently Amended) Zeolite N having a composition according to the formula

$$(M_{1-1}, P_a)_{12}(Al_bSi_c)_{10}O_{40}(X_{1-1}, Y_d)_2 nH_2O$$
 where

M = alkali metal or ammonium:

P = alkali metal, ammonium or metal cations exchanged in lieu of alkali metal or ammonium

X = halide and Y is an anion and

$$0 \le a \le 1, 1 \le c/b \le \infty t, 0 \le d \le 1 \text{ and } 1 \le n \le 10$$

with the proviso that when a = 0, b = 1, c = 1, d = 0[[,]] and X = CI, then $M \neq K$ (potassium).

- (Previously Presented) Zeolite N as claimed in claim 91, having a BET surface area greater than 1m²/q.
- (Previously Presented) Zeolite N as claimed in claim 92 having a BET surface area between 1 m²/g and 150 m²/g.
- 94. (Previously Presented) Zeoilte N having a structure as claimed in claim

 92 having a proportion of external surface area to internal surface area of greater than 1%.
- 95. (Previously Presented) Zeolite N as claimed in claim 94 having a proportion of external surface area to internal surface area of greater than 5%.
- 96. (Previously Presented) Zeolite N as claimed in claim 91 having an X-ray diffraction pattern which has a high background intensity of greater than 5% of a maximum peak helpht between the region 25° < 20 < 70°.

- 97. (Currently Amended) A method of exchanging ammonium ions in solution including the step of contacting a zeolite Zeolite N as claimed in claim 91 with a solution when used for exchange of ammonlum ions in solution.
- 98. (Currently Amended) The method of claim 97 wherein the exchange of ammonium ions in solution is carried out Zeolite N as claimed in claim 91 when used for exchange of ammonium ions in the presence of alkali metal and/or alkaline earth metal ions in solution.
- 99. (Previously Presented) Zeolite N as claimed in claim 91 having a cation exchange capacity ranging from 100 meq per 100g to 700 meq per 100g for ammonium lons with concentrations between less than 1 mg/L to greater than 10, 000 mg/L.
- 100. (Currently Amended) A method of exchanging metal ions in solution including the step of contacting a zeolite Zeolite N as claimed in claim 91 with a solution when used for exchange of metal ions in solution.
- 101. (Currently Amended) <u>The method of claim 100 wherein the exchange of metal</u> ions in solution is carried out Zeolite N as claimed in claim 91 when used for exchange of metal ions in the presence of alkali metal or alkaline earth metal ions in solution.
- 102. (Currently Amended) <u>A method of adsorbing ammonia gas including the step of contacting a zeolite</u> <u>Zeolite</u> N as claimed in claim 91 <u>with</u> when used for adsorbing ammonia gas in the temperature range 0°C to 300°C.
- 103. (Currently Amended) <u>The method of claim 102 wherein the adsorption of ammonia gas is carried out Zeolite N-as claimed in claim 91 when used for adsorbing ammonia gas in the temperature range 0°C to 300°C in the presence of water.</u>

- 104. (Currently Amended) Amethod of absorbing oil including the step of contacting a zeolite Zeolite N as claimed in claim 91 with the when used for absorbing oil.
- 105. (Currently Amended) The method of claim 104 wherein the zeolite ≥ 2colite N absorbs as claimed in claim 104 when used for absorbing oil greater than 50g of oil per 100g of zeolite Zeolite N.
- 106. (Currently Amended) <u>A method of removing anions from wastewater including</u>
 the step of contacting a zeolite Zeolite N as claimed in claim 91 with when used for removing anions within from wastewater.
- 107. (Currently Amended) A method of re-exchanging alkali metal ions from a solution containing hydroxyl ions including the step of contacting an ammonium form of a zeolite Zeolite N as claimed in claim 91 with when used in an ammonium form to have a capacity to re-exchange alkali metal ions within a solution from solutions containing hydroxyl ions ranging in concentration from 0.1 M to 2.0 M.
- 108. (Previously Presented) Zeolite N as claimed in claim 91 having a removal rate of ammonium ion ranging between 50-100% from ammonium loaded Zeolite N using a regeneration solution containing hydroxyl ions.
- 109. (Currently Amended) A method of re-exchanging ammonium ions and/or of retaining a high selectivity for ammonium ions in a zeolite N including the step of contacting a Zeolite N as claimed in claim 91 with the when used to re-exchange-ammonium ions and/or to retain high selectivity for ammonium ions after regeneration of the zeolite N with a solution containing hydroxyl ions.

- 110. (Currently Amended) A method of killing gram positive or gram negative bacteria including the step of contacting a zeolite Zeolite N as claimed in claim 91 with the when used to kill gram positive or gram negative bacteria.
- 111.(Previously Presented) Zeolite N as claimed in claim 91 where c/b is greater than 1.
- 112. (Previously Presented) Zeolite N as claimed in claim 111 where c/b has an upper value of 3.
- 113. (Previously Presented) Zeolite N as claimed in claim 111 where c/b has an upper value of 5.
- 114. (Previously Presented) Zeolite N as claimed in claim 91 where Y is hydroxyl or halide.
 - 115. (Previously Presented) Zeolite N as claimed in claim 114 where Y is chloride.